Catalytic Hydrogenation of Diacetyl Monoxime to Tetramethylpyrazine with the Soluble Transition Metal Catalysts

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Abstract: Catalytic hydrogenation of diacetyl monoxime to tetramethylpyrazine, by the homogeneous catalysts generated *in situ* from some transition metal chlorides with triphenylphosphine in ethanol under H₂ pressure of $0.6 \sim 4.6$ MPa at $100 \sim 150$ °C, has been studied. The optimum H₂ partial pressure was observed at about 1.3 MPa. The maximum conversion of diacetyl monoxime and yield of tetramethylpyrazine were 97% and 90%, respectively.

Keywords: Diacetyl monoxime, catalytic hydrogenation, tetramethylpyrazine.

Tetramethylpyrazine (TMP) is a useful compound in food industry¹. In recent years it has been found as an active ingredient in Chuanxiong (*ligusticum wallichii franch*), which is a traditional Chinese herb. Now TMP has been widely used in the treatment of patients with cerebral ischemic diseases in China². One of the important methods for the preparation of tetramethylpyrazine is the self-condensation of two molecules of 2-amino butanone to 2, 5-dihydrotetramethlipyrazine and subsequent oxidation to TMP³. 2-Amino butanone is prepared usually *in situ via* the reduction of the corresponding diacetyl monoxime by reducing agents, such as zinc-alkali, zinc-acetic acid, *etc*³. Whereas homogeneous catalytic hydrogenation routes of diacetyl monoxime (DAM) have been scarcely explored. In the present work, we wish to report the synthesis of tetramethylpyrazine *via* catalytic hydrogenation of diacetyl monoxime using homogeneous transition metal catalysts.

IR spectra were obtained on a MAGNA IR-560 spectrometer. ¹H NMR spectra were determined with $Me_3Si-SiMe_3$ as an internal standard in CCl_4 solvent on a PMX-60M Hz instrument. UV-VIS spectra were recorded with a Shimadzu UV-2401 spectrophotometer. MS spectra were determined with a Finnigan Mat Magnum GC/MS ion trap system.

The catalytic hydrogenation was carried out in a 24 ml glass-lined stainless steel autoclave. A mixture of $PdCl_2$ (2.91 mg, 1.63×10^{-2} mmol), PPh_3 (6.3 mg, 2.45×10^{-2} mmol), DAM (0.5 g, 4.89 mmol) and ethanol (6 ml) were added into the autoclave. The reactor was purged five times with hydrogen, before setting the required H₂ pressure. Hydrogen up to 1.3 MPa was introduced and the reaction vessel was placed in a preheated thermostatic oven which could be agitated by shaking (12 times / min.). The

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reaction mixture was kept at 150 °C for 6 h. After being cooled to room temperature, the reaction solution was immediately analyzed and identified by GC-MS and UV-VIS. In the meantime, the products were isolated and purified by preparative TLC on silica gel (Cyclopentane: ethyl acetate = 2:1), and further identified by H¹-NMR, IR and melting point determining. The data of TMP are in accord with refs^{3, 4}.

During our investigation of the catalytic hydrogenation of DAM with hydrogen using homogeneous palladium chloride-triphenylphosphine catalytic systems, we found incidentally that the reaction shown by **Scheme 1** could take place more easily to TMP under lower H_2 pressure⁵. Besides PdCl₂-PPh₃, Co, Ni, Pt, and Fe analogues can also be used as catalysts (**Table1**). But the PdCl₂ - PPh₃ catalytic systems gave the maximum

Scheme 1.

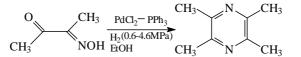


Table 1. The reaction results^a

Catalyst precursor	PPh ₃ /M	T (℃)	P _{H2} (MPa)	t (h)	Conversion (%)	Yield ^b (%)
PdCl ₂ , PPh ₃	1.5	150	1.3	6	97	90
PdCl ₂ , PPh ₃	1.5	120	4.0	6	87	53
CoCl ₂ , PPh ₃	3.0	150	2.4	25	76	72
CoCl ₂ , PPh ₃	3.0	100	4.0	30	67	57
NiCl ₂ , PPh ₃	3.0	150	4.0	18	96	56
NiCl ₂ , PPh ₃	3.0	120	4.0	26	37	31
H ₂ PtCl ₄ , PPh ₃	3.0	150	4.0	6	64	49
H ₂ PtCl ₄ , PPh ₃	3.0	120	3.0	16	40	40
FeCl ₃ , PPh ₃	3.0	150	1.0	6	27	24
FeCl ₃ , PPh ₃	3.0	120	4.0	46	25	13
RuCl ₃ , PPh ₃	3.0	120	4.0	26	4	2

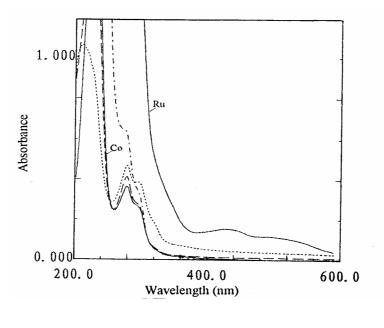
a. Other conditions: DAM 0.5 g, DAM/metal chloride: 300 (mole ratio), EtOH 6 ml.

b. Yields were determined by GC-MS analysis.

yield 90% of TMP. The activities of the various transition metals are in the order: Pd > Pt > Co > Ni > Fe > Ru. The tendency appears to be related to the stability of the complexes generated from the corresponding transition metal chlorides with DAM. Atchay *et al* reported that $Pd^{(II)}$, $Co^{(II)}$, $Ni^{(II)}$ and $Fe^{(II)}$ could form unstable complexes with DAM^{5,6}, the stability of these complexes were in the opposite order: Pd < Co < Ni < Fe. In order to find out whether the metals could form the complexes with DAM during the reaction, we determined the electronic spectra of their reaction mixtures (**Figure1**). Most of catalytic systems had no absorption band in the region of $400 \sim 600$ nm, but the peaks at 279 and 295 nm were assigned to the characteristic absorption of TMP⁴. Only Ru-PPh₃ reaction system had two absorption peaks at 439 and 500 nm, which were assigned to the absorbance of charge-transfer transition bands from Ru^(II) to DAM in the complexes⁸. This result indicated that the formation of stable Ru-DAM complexes retarded the further reaction proceeding. So the RuCl₃ -PPh₃ catalytic system displayed

poor activity in the reaction.

Figure 1. Electronic spectra of the reaction solution after hydrogenation of DAM catalyzed by transition metal-triphenylphosphine catalytic systems^{a,b}



- $\begin{array}{l} \text{Ru-PPh}_3 \mbox{ (Ru---), Pt-PPh}_3 \mbox{ (----), Ni-PPh}_3 \mbox{ (----), Pd-PPh}_3 \mbox{ (----), Co-PPh}_3 \mbox{ (Co----)} \end{array}$
- a. The electronic spectra were obtained at 25 °C.
- b. Reaction conditions: see experimental section

It was also found that H_2 pressure dramatically changed the reaction results shown in **Figure 2**. The conversion of DAM increased with increasing H_2 pressure in lower pressure range; while the conversion remained nearly constant when H_2 pressure is higher than 1.3 MPa. However a new trend for the yield of TMP was observed, the yield of TMP passed through a maximum at H_2 pressure of 1.3 MPa. Similar trends can be also observed in the systems of Co, Ni, and Pt. We think the phenomena match well with the following reaction path (**Scheme 2**). The conversion of DAM to TMP proceeds actually in three discrete steps: (i) hydrogenation of DAM to yield 2-amino butanone (**a**); (ii) condensation of **a** to form dihydrotetramethylpyrazine (**b**); (iii) dehydrogenation of **b** to afford TMP. It is clear that the effect of H_2 pressure on the first step is opposite to the third step. Increasing H_2 pressure is in favor of the hydrogenation of DAM to **a**, but not of the dehydrogenation of **b**. So the optimum H_2 pressure was observed at about 1.3 MPa.

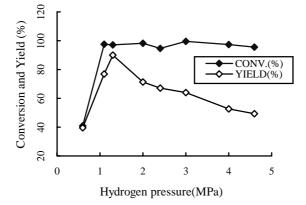
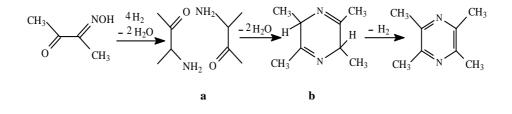


Figure 2. Effect of H₂ pressure on the reaction results of PdCl₂-PPh₃ catalytic systems





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